

Communication

# Methane to Methanol Conversion Using Proton-Exchange Membrane Fuel Cells and PdAu/Antimony-Doped Tin Oxide Nanomaterials

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**Abstract:** This study investigates the use of Au-doped Pd anodic electrocatalysts on ATO support for the conversion of methane to methanol. The study uses cyclic voltammetry, in situ Raman spectra, polarization curves, and FTIR analysis to determine the optimal composition of gold and palladium for enhancing the conversion process. The results demonstrate the potential for utilizing methane as a feedstock for producing sustainable energy sources. The Pd<sub>75</sub>Au<sub>25</sub>/ATO electrode exhibited the highest OCP value, and Pd<sub>50</sub>Au<sub>50</sub>/ATO had the highest methanol production value at a potential of 0.05 V. Therefore, it can be concluded that an optimal composition of gold and palladium exists to enhance the conversion of methane to methanol. The findings contribute to the development of efficient and sustainable energy sources, highlighting the importance of exploring alternative ways to produce methanol.

**Keywords:** methane conversion; fuel cell; methanol; PEM; PdAu/ATO



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## 1. Introduction

Methane is a widely available and inexpensive source of energy, but its combustion for energy production releases CO<sub>2</sub>, contributing to climate change [1]. Therefore, researchers are exploring alternative methods to convert methane into chemicals like methanol, which can be utilized as a clean fuel and has diverse industrial applications [2]. Various techniques have been developed for methane conversion, including homogeneous and heterogeneous catalysis, photocatalysis [3], biocatalysis, plasma technologies, and electrochemical processes [4–7]. Among these, electrochemical processes have shown promise for converting methane into methanol under mild conditions and generating electricity [8–11].

To co-generate chemicals and electricity, one possible approach is to use a polymer electrolyte fuel cell as a reactor for converting methane into methanol and formates [11,12]. However, this conversion is challenging due to the high strength of the C-H bond in methane (434 kJ·mol<sup>-1</sup>) and its low polarizability because of its regular tetrahedron conformation [13]. Therefore, the process involves oxidizing methane through a non-faradaic reaction, which activates methane using more reactive species generated via faradaic processes, such as reactive oxygen species (ROS) from water activation. The significance of water activation in transferring oxygen to hydrocarbon molecules to produce methanol has been emphasized by researchers [14–16].

To achieve this conversion, catalysts with specific characteristics are required. One of the key requirements is for the catalysts to have a bifunctional effect [17–19], that is, to be able to adsorb methane and activate water molecules. While transition metal oxides are commonly used catalysts, researchers have been exploring alternative catalysts, such as platinum and palladium, which have shown promising results in methane oxidation to methanol [11,20].

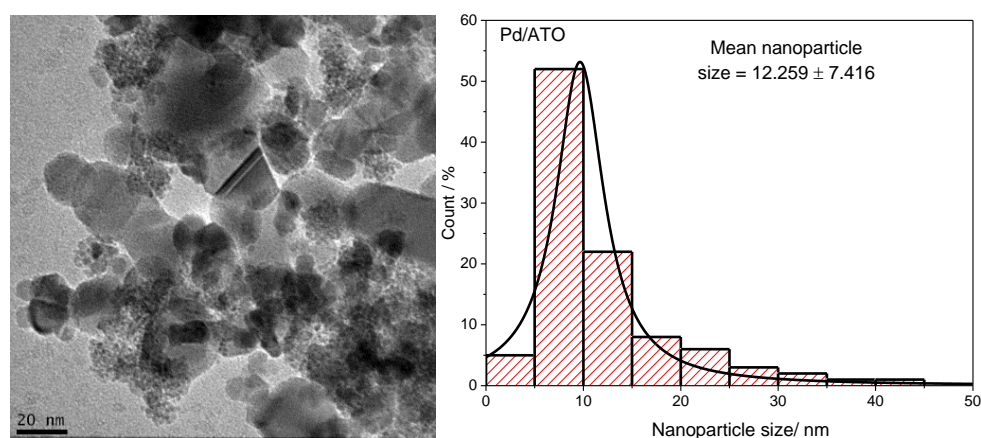
Palladium- and gold-supported carbon materials, such as carbon nanotubes, activated carbon, and reduced graphene oxide [21,22], have been identified as effective catalysts for this process. Pd-Au nanoparticles have been used as active centers, and their catalytic activity can be improved by supporting them on functionalized carbon nanotubes [23]. In addition, gold's affinity for oxygen can facilitate the breakdown of hydrogen peroxide into  $\text{OH}\bullet$ , which activates the C-H bond [21,24,25].

On the other hand, the oxygenated species produced can also attack the catalyst support, typically carbon, which affects the reactor's durability. Recent studies have explored the use of metallic oxides like  $\text{TiO}_2$  and antimony-doped tin oxide (ATO) as catalyst support to improve catalyst stability [26–28]. In this context, this study investigated the conversion of methane to methanol in a polymer electrolyte fuel cell using Au-doped palladium anodic electrocatalysts in different proportions on an ATO (antimony-doped tin oxide) support. ATO was selected as the support because it promotes the formation of reactive oxygen species, and has good electrical conductivity and corrosion resistance, making it a promising catalyst support option for the methane-to-methanol reaction [29–32].

## 2. Results

Figure 1 presents microscopy images and nanoparticle size distribution histograms for Au/ATO, Pd/ATO, and PdAu/ATO with varying ratios. The average nanoparticle size ranges from 12 to 19 nm, with the smallest size (12 nm) observed in the Pd/ATO catalyst and the largest size (19 nm) observed in the  $\text{Pd}_{50}\text{Au}_{50}$ /ATO catalyst. Additionally, the images show that the nanoparticles are not well dispersed on the support and tend to agglomerate. The ATO support's ability has been observed in other catalytic materials in the literature [29–35].

X-ray diffraction (XRD), as shown in Figure 2a, was utilized to characterize the chemical structures of a series of Pd/ATO, Au/ATO, and PdAu/ATO samples. The peaks observed at  $2\theta \approx 26^\circ, 33^\circ, 38^\circ, 51^\circ, 54^\circ, 62^\circ,$  and  $64^\circ$  correspond to the characteristic diffraction peaks of  $\text{SnO}_2\cdot\text{Sb}_2\text{O}_5$  (JCPDS# 88-2348). The palladium and gold peaks appear discretely in comparison. Based on the diffraction pattern with intensity normalized by the logarithmic function (Figure 2b), it was possible to clearly observe the characteristic peaks of Pd and Au. The Pd-related peaks at  $2\theta \approx 38^\circ, 49^\circ,$  and  $66^\circ$  are associated with the crystalline planes (111), (200), and (311), according to (JCPDS# 89-4897), which reveals a face-centered cubic (FCC) structure for Pd/ATO. The relative intensities of Pd and ATO are still discrete, even when normalized on a logarithmic scale, reflecting the smaller particle size compared to the other materials.



(a)Pd/ATO

Figure 1. Cont.

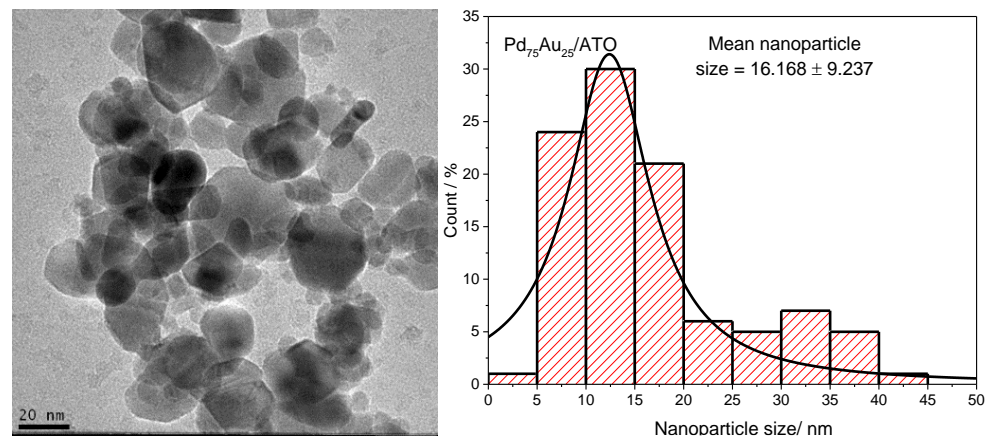
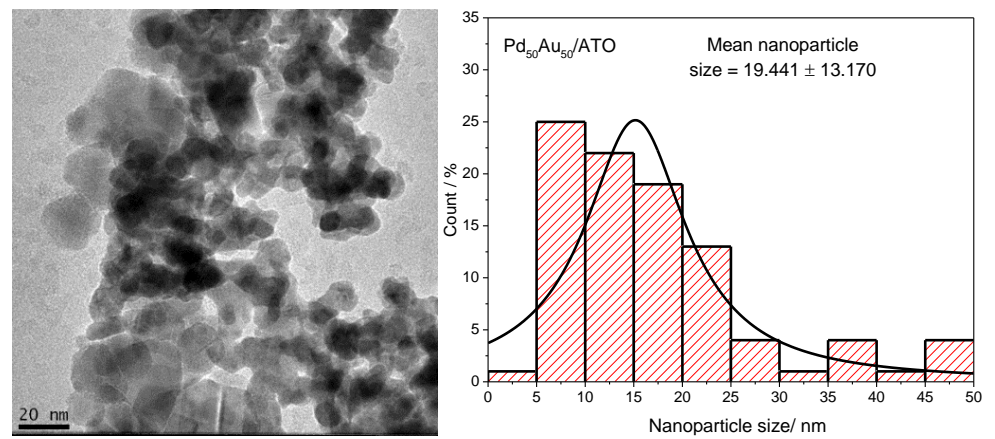
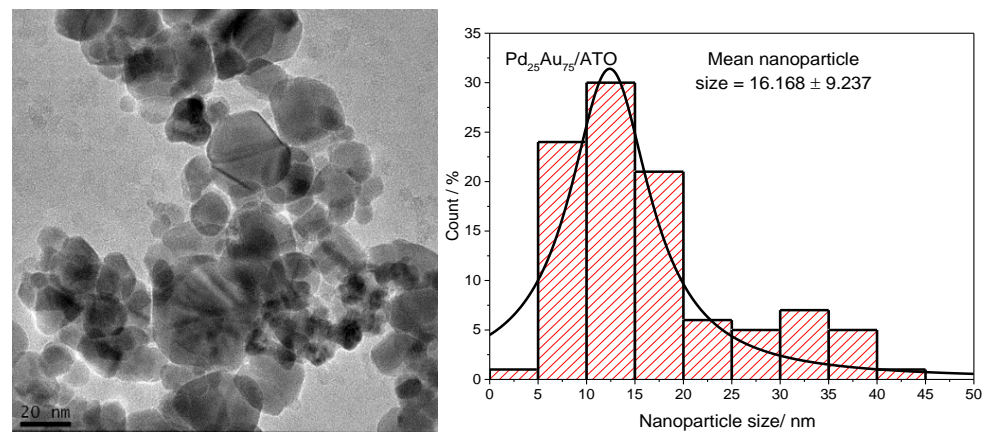
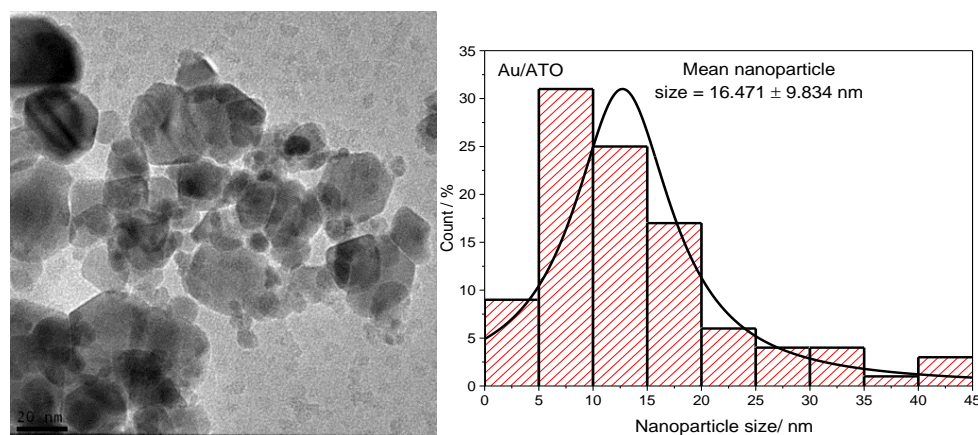
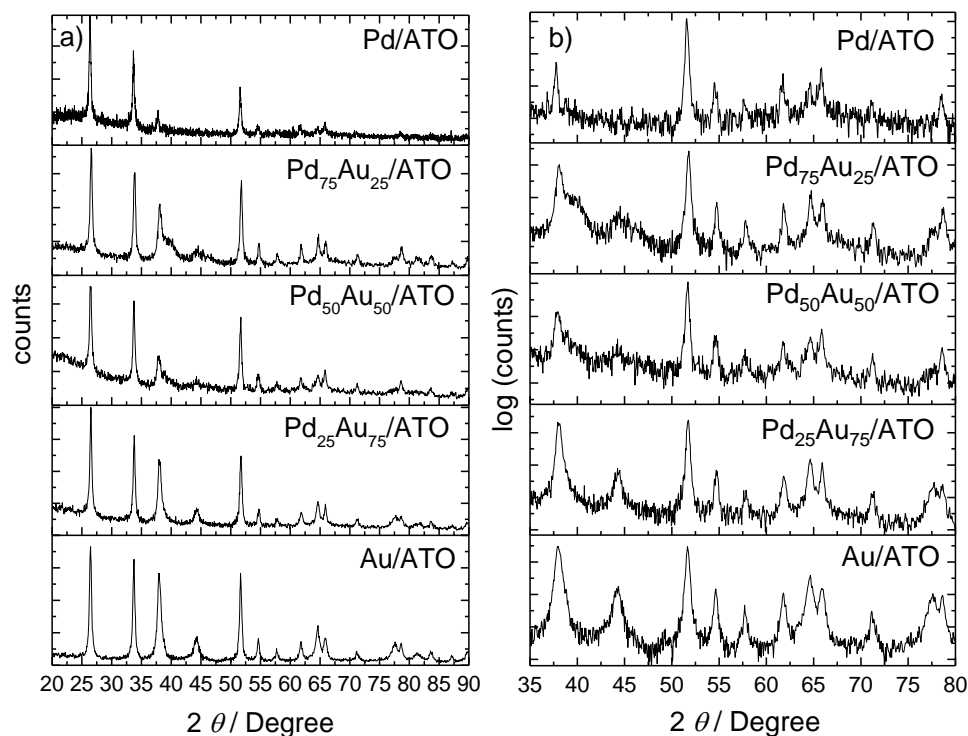
(b)Pd<sub>75</sub>Au<sub>25</sub>/ATO(c)Pd<sub>50</sub>Au<sub>50</sub>/ATO(d)Pd<sub>25</sub>Au<sub>75</sub>/ATO

Figure 1. Cont.



(e) Au/ATO

**Figure 1.** TEM micrographs and histograms of nanoparticle size distributions in, (a) Pd/ATO, (b) Pd<sub>75</sub>Au<sub>25</sub>/ATO, (c) Pd<sub>50</sub>Au<sub>50</sub>/ATO, (d) Pd<sub>25</sub>Au<sub>75</sub>/ATO and (e) Au/ATO.



**Figure 2.** X-ray diffractogram (XRD) patterns of Au/ATO, Pd/ATO, and PdAu/ATO in different ratios. (b) Logarithm of the intensities of the diffractograms in (a).

Two small reflection peaks were observed at  $2\theta \approx 38.1^\circ$  and  $44.4^\circ$ , corresponding to the (1 1 1) and (2 0 0) planes of face-centered cubic-structured Au (JCPDS no. 89-3697). The peaks relative to the (2 2 0) and (3 1 1) planes at  $2\theta \approx 64^\circ$  and  $77^\circ$ , respectively, appear convoluted with the peaks of Pd and tin oxide. It is noteworthy that the peak with the (3 1 1) plane stands out.

The cyclic voltammetry of PdAu materials, in different molar ratios in  $1.0 \text{ mol L}^{-1}$  NaOH aqueous solution (scan rate  $v = 10 \text{ mV s}^{-1}$ ), is presented in Figure 3a. In the materials containing Pd, it is possible to observe in the region of  $-0.85$  and  $-0.5 \text{ V}$  the peaks corresponding to hydrogen adsorption and desorption [36], the Pd/ATO electrode presenting the oxide reduction ( $-0.4 \text{ V}$ ), and oxide formation ( $0.05 \text{ V}$ ). The PdAu/ATO

electrodes show a shift in the peak positions for the hydrogen adsorption–desorption, compared to Pd/ATO, which indicates the electronic modification of Pd atoms by Au [37].

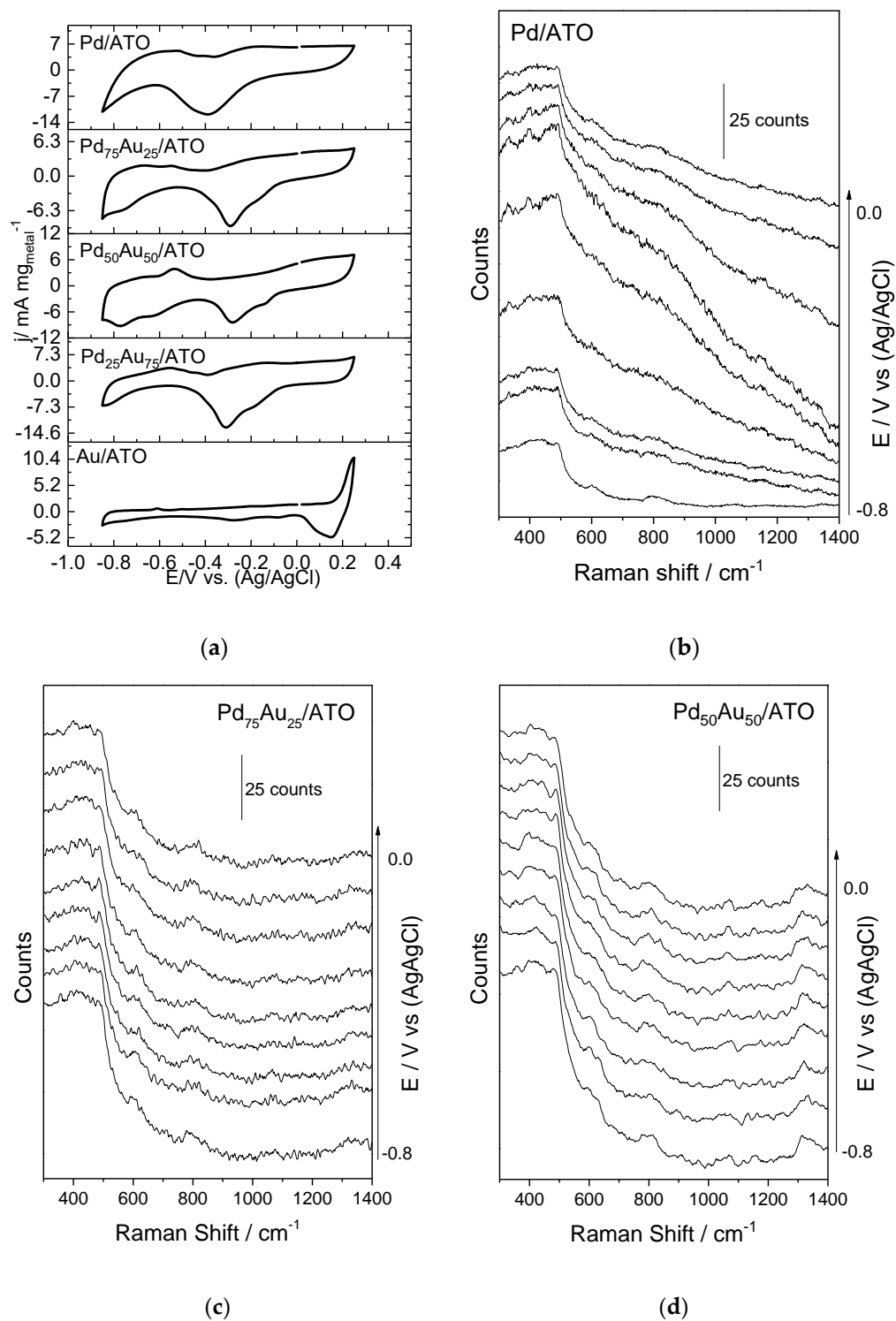
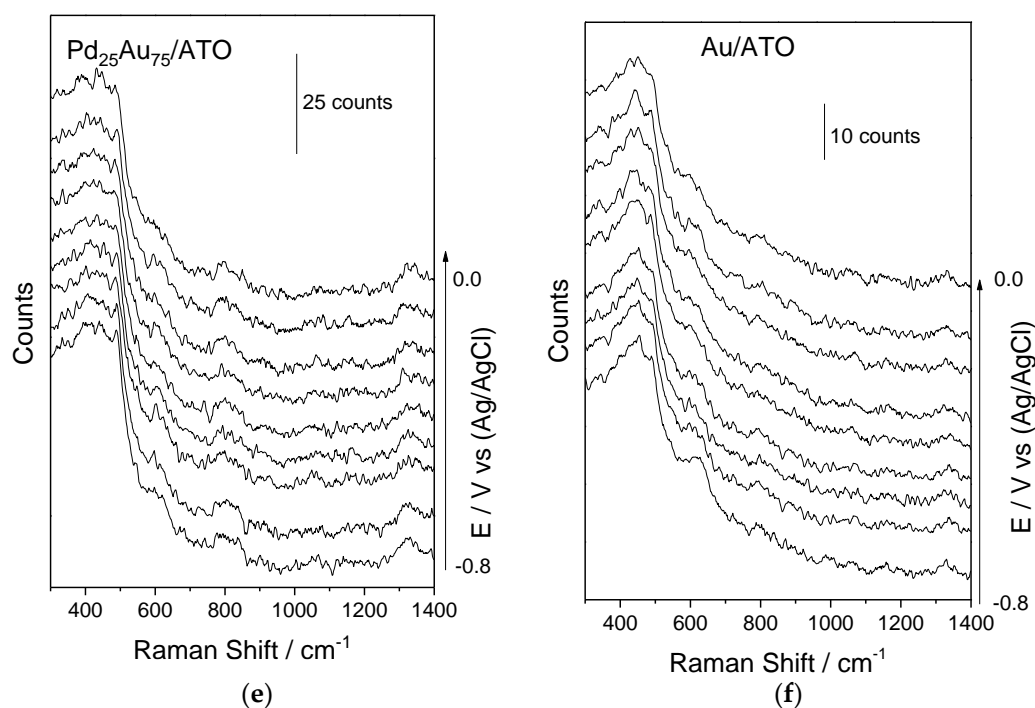


Figure 3. Cont.

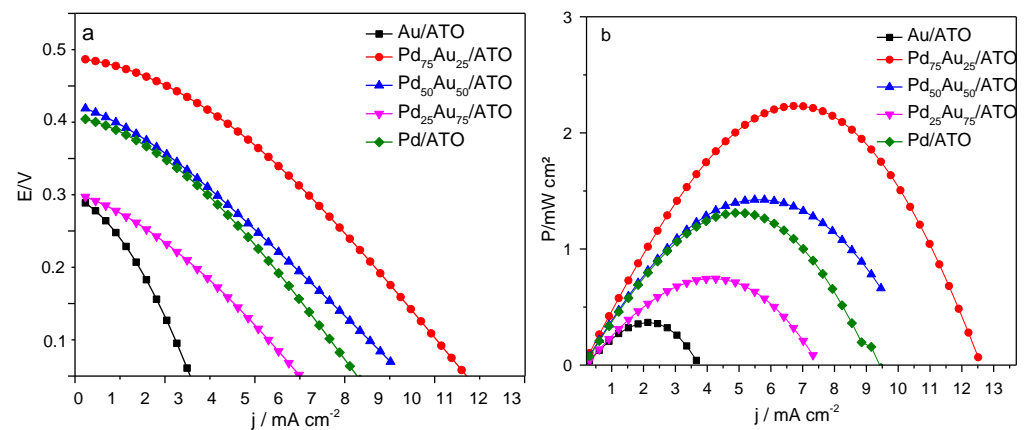


**Figure 3.** (a) Cyclic voltammetry (CV) of Au/ATO, Pd/ATO, and PdAu/ATO in different ratios (scan rate  $v = 10 \text{ mV s}^{-1}$ ) in  $1 \text{ mol L}^{-1}$  NaOH aqueous solution. (b–f) Spectra of in situ Raman-assisted electrochemical measurements collected at different potentials in NaOH  $1.0 \text{ mol L}^{-1}$ .

The presence of gold sites near palladium sites can alter the chemical environment and shift the hydrogen desorption potential to less negative values with an increase in the gold content in the material ( $-0.55$ ,  $-0.57$ , and  $-0.59 \text{ V}$  for  $\text{Pd}_{75}\text{Au}_{25}/\text{ATO}$ ,  $\text{Pd}_{50}\text{Au}_{50}/\text{ATO}$ , and  $\text{Pd}_{25}\text{Au}_{75}/\text{ATO}$ , respectively). In order to complement and expand the observations from cyclic voltammetry, in situ Raman spectra of the Pd-Au materials were measured (Figure 3b). In all of the spectra, the characteristic bands of  $\text{SnO}_2$  are observed at approximately  $486$ ,  $602$ , and  $780\text{--}793 \text{ cm}^{-1}$ , corresponding to the active bands of  $\text{SnO}_2$  Eg,  $A_{1g}$ , and  $B_{2g}$ , respectively [38,39]. Additionally, a band centered at  $639 \text{ cm}^{-1}$ , corresponding to the bending of the PdO-H bond [40], indicates the oxidation of Pd as a function of potential in the Pd/ATO catalyst.

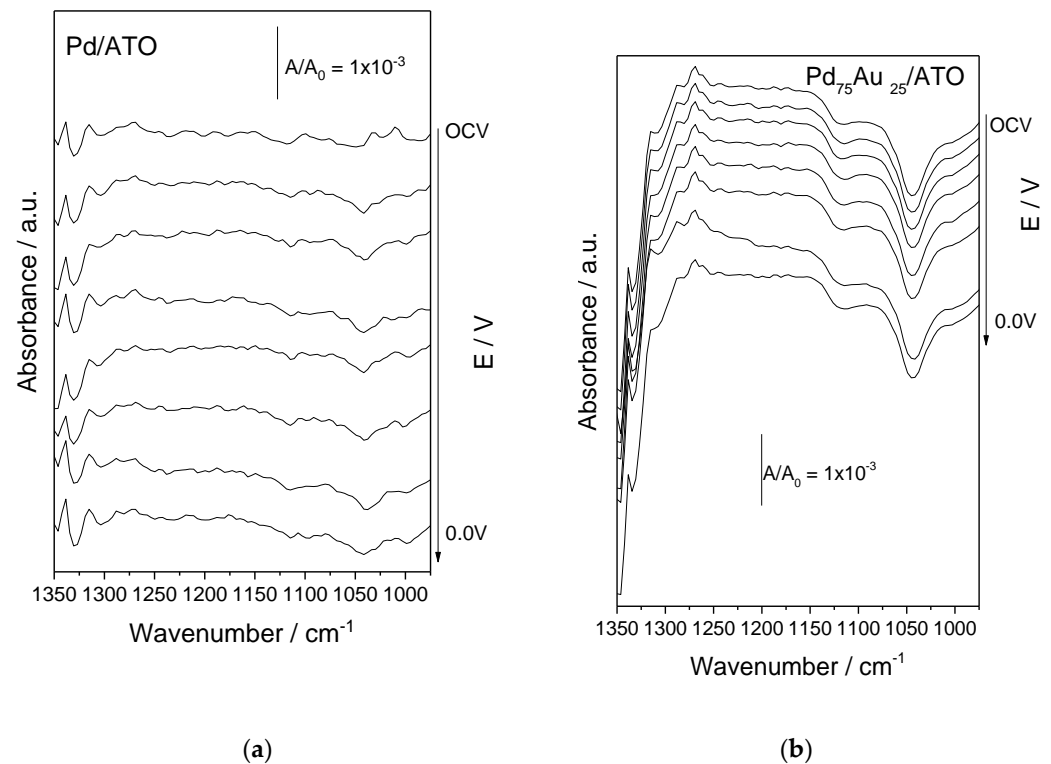
For all materials containing gold, it is possible to observe a feature at potentials less negative than  $-0.4 \text{ V}$ , which is assigned to the Au-O stretching vibration of Au oxide and appears at approximately  $559 \text{ cm}^{-1}$  [41], and this potential is shifted for more negative values as the gold content increases. The  $635 \text{ cm}^{-1}$  band refers to the Au-O and Au-OOH vibrations [42], and this band decreases with the addition of Pd. The band observed at  $602 \text{ cm}^{-1}$  in  $\text{SnO}_2$  overlapped with this band, while distinct bands were observed at  $794$ ,  $974$ , and  $1166 \text{ cm}^{-1}$ , which can be attributed to Nafion [43].

The polarization curves (Figure 4) of the partial oxidation of methane in a polymer electrolyte reactor and the measured open circuit potential (OCP) values range between  $0.3$  and  $0.5 \text{ V}$ , which are comparable to those reported in the other literature [3,29]. The  $\text{Pd}_{75}\text{Au}_{25}/\text{ATO}$  electrode exhibits the highest OCP value, while the Au/ATO electrode has the lowest, indicating that the synergy between Pd and Au increases the OCP value compared to that of Pd or Au alone. The Au/ATO and  $\text{Pd}_{25}\text{Au}_{75}/\text{ATO}$  electrodes have the same OCP value, but the power density of  $\text{Pd}_{25}\text{Au}_{75}/\text{ATO}$  is  $0.9 \text{ mW/cm}^2$ , which is higher than that of Au/ATO ( $0.49 \text{ mW/cm}^2$ ). The results indicate that the addition of gold to palladium can favor the generation of methane oxidation products through reactive oxygen species, which in turn can be oxidized by Pd. Since the oxidation potentials of methanol and formic acid are lower than the water activation potential, they can lead to an increase in the open circuit potential.

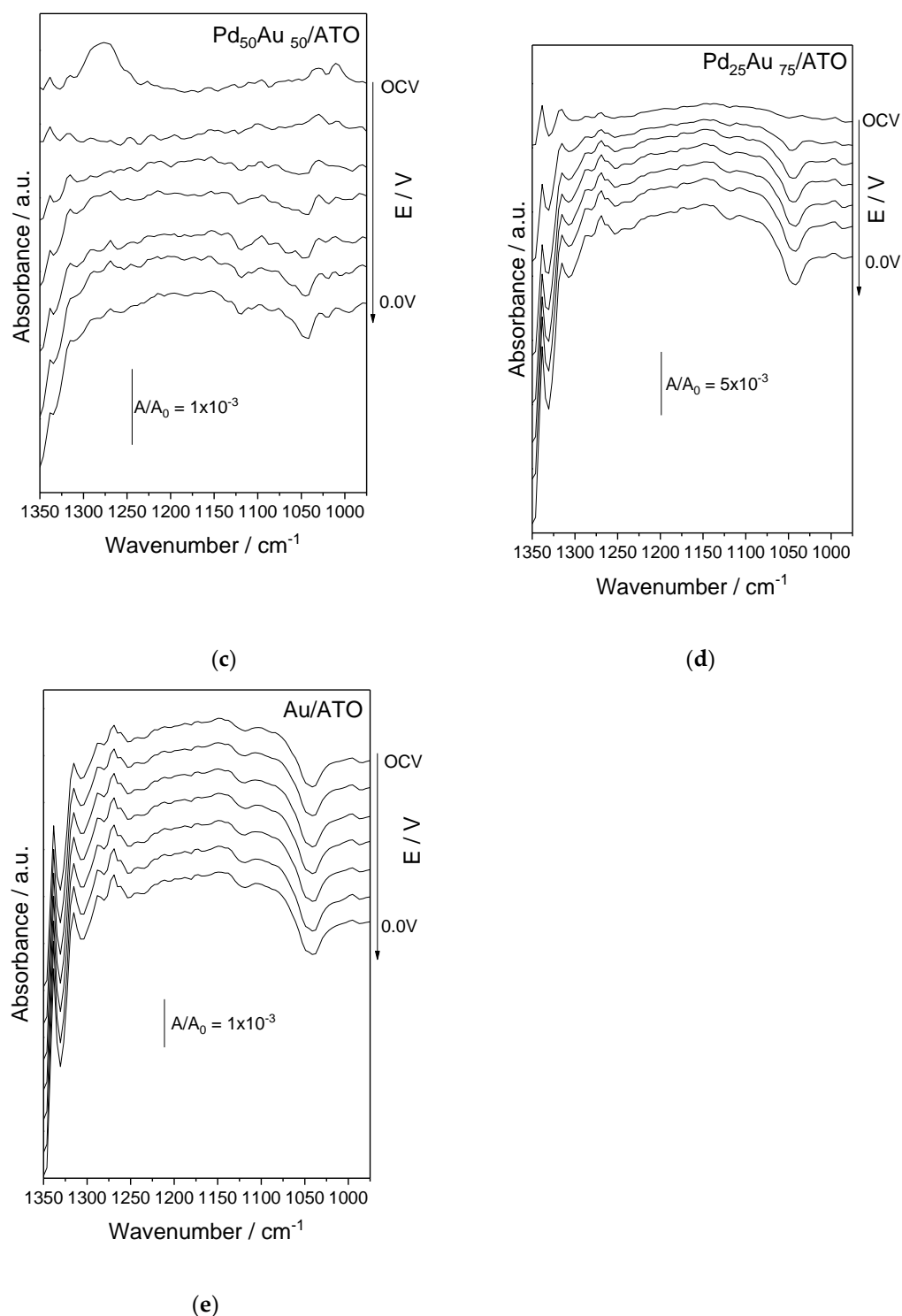


**Figure 4.** (a) Polarization curves of ATO-supported PdAu materials in different compositions. (b) Power density curves.

The FTIR analysis (Figure 5) displays the spectra of aliquots collected from the reactor effluent every 100 mV for 5 min in a  $1.0 \text{ mol L}^{-1}$  NaOH solution, with a methane flow rate adjusted to  $100 \text{ mL min}^{-1}$  for all of the catalysts. The obtained spectra exhibit a characteristic methane band at  $\sim 1304 \text{ cm}^{-1}$ , corresponding to  $\text{CH}_4$  dissolving in water [44,45]. Methanol formation can be identified by specific bands that appear at 1033, 1077, and  $1082 \text{ cm}^{-1}$  [46], although they are subtle and present in all materials. Additionally, a band centered at  $\sim 1342 \text{ cm}^{-1}$  corresponding to the  $\nu(\text{COO})$  of formate in the solution [47] is visible in all of the materials. This band may indicate that the process is leading to more oxidized products of methane than methanol. The presence of formic acid peaks in the gold-content materials already at the OCP indicates the production of more oxidized products even at the lowest possible overpotentials at the anode.



**Figure 5.** Cont.



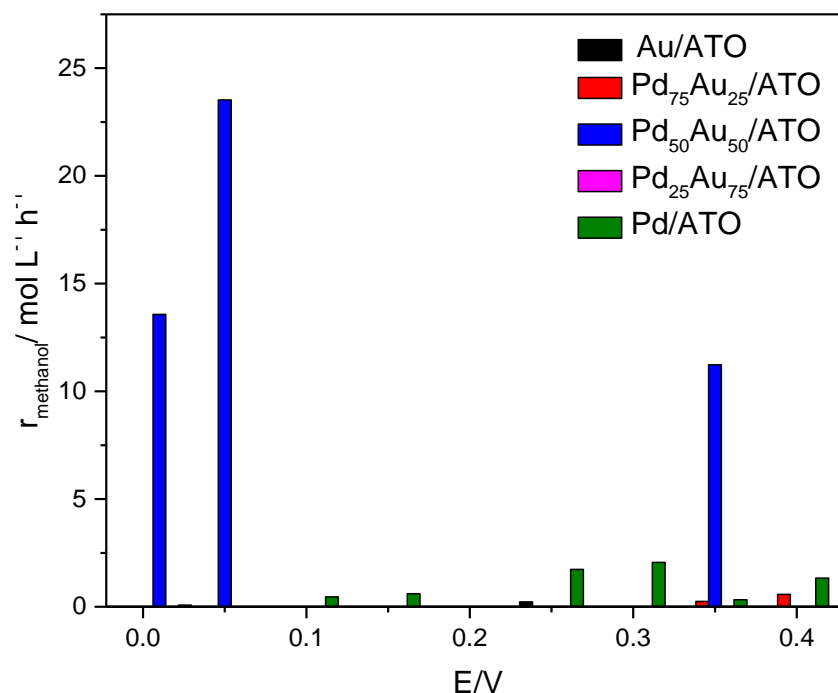
**Figure 5.** Spectra of FTIR aliquots collected from the reactor effluent every 100 mV for 5 min in presence of  $\text{NaOH } 1.0 \text{ mol L}^{-1}$ , with methane flow adjusted to  $100 \text{ mL min}^{-1}$  for (a) Pd/ATO, (b)  $\text{Pd}_{75}\text{Au}_{25}/\text{ATO}$ , (c)  $\text{Pd}_{50}\text{Au}_{50}/\text{ATO}$ , (d)  $\text{Pd}_{25}\text{Au}_{75}/\text{ATO}$  and (e) Au/ATO in potentials of  $-0.4$ ;  $-0.3$ ;  $-0.2$ ;  $-0.1$  and  $0.0 \text{ V}$ .

The collected effluent from the reactor was also used to quantify the methanol produced via HPLC, and this value was converted and reported as the rate of reaction (Equation (1)).

$$r = ([\text{methanol}]) / (V \cdot \text{time}) \quad (1)$$



Figure 6 reports the rate of reaction for palladium- and gold-based materials. The data show that Pd<sub>50</sub>Au<sub>50</sub>/ATO has the highest methanol production value at a potential of  $-0.05$  V, outperforming all of the other materials and potentials. These results indicate that an optimal composition of gold and palladium exists to enhance the conversion of methane to methanol. The combination of gold's oxophilic nature [21,22], which facilitates water activation, with PdO's carbophilic ability [11], and the balance between the two types of sites, favors the pathway of methane conversion to methanol.



**Figure 6.** Rate reaction of Au/ATO, Pd/ATO, and PdAu/ATO in different potentials.

The observed results for Pd<sub>50</sub>Au<sub>50</sub>/ATO are up to 3 times higher than those reported in the literature for PdNi ( $\sim 8$  mol L<sup>-1</sup> h<sup>-1</sup>) [29]. There is no formation of methanol in measurable quantities for Pd<sub>25</sub>Au<sub>75</sub>/ATO.

### 3. Materials and Methods

The PdAu/ATO materials were synthesized using the sodium borohydride reduction method [28] with varying ratios. To prepare each material, a solution of ultrapure water and isopropanol (50/50 *v/v*) was mixed with a specific amount of ATO support (Sb<sub>2</sub>O<sub>5</sub>•SnO<sub>2</sub> Aldrich) in an ultrasonic bath for 15 min. Subsequently, 20% of metallic precursors Pd(NO<sub>3</sub>)<sub>2</sub>•2 H<sub>2</sub>O (Aldrich) and HAuCl<sub>4</sub>•3 H<sub>2</sub>O (Aldrich) was added in different ratios. In this medium, NaBH<sub>4</sub> (Aldrich) was added to a 10 mL 0.01 mol L<sup>-1</sup> NaOH solution with an excess of 5:1 in relation to the metals, and stirring was maintained for 30 min. The resulting material was then washed and filtered using 4 L of ultrapure water (18 MΩ cm<sup>-1</sup>).

The morphology of PdAu/ATO (nanoparticle size and general aspects) was investigated using transmission electron microscopy (TEM) via JEOL JEM-2100, operated at 200 keV. For the histogram and the calculation of the average size, 300 nanoparticles of each catalyst were calculated using the ImageJ software package. The crystalline structure of the materials was analyzed using a diffractometer (Rigaku–Miniflex II) at Cu/ $\alpha$   $\lambda = 0.154$  nm, with  $2\theta$  ranging from 20 to 90°, with a scan speed of 2° min<sup>-1</sup>, operating at 40 kV. The analyzed XRD standards were compared with those of JCPDS (Joint Committee on Powder Diffraction).

The electrochemical experiments were observed via cyclic voltammetry (CV) performed on a three-electrode cell, connected to a potentiostat/galvanostat (PGSTAT 302 N,

Autolab<sup>®</sup>), with PdAu/ATO as the working electrode, a 2 cm<sup>2</sup> Pt plate as the counter electrode, and a commercial Ag/AgCl electrode (3.0 mol L<sup>-1</sup> solution) as the reference electrode, all in a single compartment cell. The Raman in situ spectra were analyzed using a Raman Micro Spectrometer—Horiba—with a 785 nm laser and the same single compartment cell used in the CV experiments.

A PEM fuel cell unit was used in this work, similar to that applied in previous studies [29,30]. Five different membrane electrode assemblies (MEAs) of anode/electrolyte/cathode were constructed. Different 1 mg per cm<sup>2</sup> of metals (Pd:Au) were used as the anode, a membrane of Nafion<sup>®</sup> 117 (DuPont<sup>®</sup>) treated with KOH was used as the electrolyte, and 1 mg of Pt/C—BASF (20% *w/w*) was used as the cathode. The ink contains the catalyst with 30% of the mass of a solution of Nafion<sup>®</sup> D-520 (Aldrich) and isopropanol. The anodes were prepared by brushing the ink on carbon cloth treated with PTFE [31,32]. The conditions of the fuel cell were fed with a mixture of methane (100 mL min<sup>-1</sup>) and NaOH 1 mol L<sup>-1</sup> at a (1 mL min<sup>-1</sup>) supply at the anode, while the cathode was supplied with a humidified O<sub>2</sub> bottle at a temperature of 85 °C with a flow rate of 400 mL min<sup>-1</sup>. The temperature measurement in the cell was 45 °C. For the application of currents and potentials to the cell, a potentiostat/galvanostat (PGSTAT 302 N, Autolab<sup>®</sup>) was used.

The reaction products were collected from the reactor every 5 min in the open circuit potential (OCP) until 0.0 V and analyzed using infrared (IR) spectroscopy performed on a Nicolett<sup>®</sup> 6700 with ATR Miracle (Pike) accessory, diamond/ZnSe crystal, and a detector of MCT, as well as high-performance liquid chromatography (HPLC) (YL9100) with a UV/Vis detector at 225 nm and flow of 0.8 mL min<sup>-1</sup> of 50% water, 40% acetonitrile, and 10% buffer solution in an isocratic run on a C18 (Phenomenex Luna 5 µm, 250 × 4.6 nm). The calibration curve presents the following linear equation: peak area = 0.29574 + 0.00979 [methanol] and presents  $r^2 = 0.994$ .

#### 4. Conclusions

This study examined the conversion of methane to methanol in a polymer electrolyte fuel cell using Au-doped palladium anodic electrocatalysts in different proportions on an ATO support. The cyclic voltammetry and in situ Raman spectra of the Pd-Au materials were measured to observe the electronic modification of Pd atoms by Au. The polarization curves of the partial oxidation of methane in a polymer electrolyte reactor and the measured open circuit potential values were also studied. The results showed that the Pd<sub>75</sub>Au<sub>25</sub>/ATO electrode exhibited the highest OCP value, probably due to gold promoting the formation of methane oxidation products through reactive oxygen species, which can subsequently be oxidized by Pd. Due to the lower oxidation potentials of methanol and formic acid compared to the water activation potential, their presence can result in an increase in the open circuit potential. The optimal activation of water in conjunction with Pd sites provided by the Pd<sub>50</sub>Au<sub>50</sub>/ATO material led to the highest methanol production. Therefore, it can be concluded that an optimal composition of gold and palladium exists to enhance the conversion of methane to methanol. This study contributes to the development of efficient and sustainable energy sources by utilizing methane, a potent greenhouse gas, as a feedstock for producing methanol.

**Author Contributions:** Conceptualization, A.O.N. and R.F.B.d.S.; methodology, A.O.N. and R.F.B.d.S.; validation, M.H.G. and V.A.M.; formal analysis, V.A.M.; investigation, V.A.M.; resources, V.A.M.; writing—original draft preparation, V.A.M.; writing—review and editing, J.N., R.F.B.d.S. and A.O.N.; supervision, A.O.N. and R.F.B.d.S.; project administration, A.O.N.; funding acquisition, A.O.N. All authors have read and agreed to the published version of the manuscript.

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**Conflicts of Interest:** The authors declare no conflict of interest.

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